DEVELOPMENT OF EARLY WARNING MODELING SYSTEM FOR SUDDEN CHEMICAL SPILL IN PLAIN RIVER NETWORK

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Key words: hydrodynamic model, water quality model, oil spill, hydrophobic model, hydrophilic model, river network.

ABSTRACT

An early warning modeling system for assessing potential river water quality threat from sudden chemical discharge incidents was developed, based on a hydrodynamic model for tidal plain river network equipped with sluice gates and water quality models. For the hydrodynamic model, the mode to simulate river flow under artificial irreversible gate operation was presented, so that the flow related to gate control with tidal occurrence could be simulated, which was calibrated by the measured data. For the water quality models, three kinds of models including oil spill model, hydrophobic model and hydrophilic model were developed based on chemical properties. With China’s Shanghai river network waters as the domain, oil spill scenario and hexachlorobenzene (HCB) spill scenario representing hydrophobic chemical were simulated based on the verified model parameters, and showed the application of the developed early warning modeling system.

I. INTRODUCTION

To tackle the sudden water pollution incident effectively, the early warning modeling is of increasing concern so as to guide environmental engineers and planners in designing and carrying out effective clean-up operations. Among these models, many focus on the fate and surface movement of oil spill. Several advanced oil-spill modeling systems have been developed such as OILMAP [13-15], OSIS [7, 9] and OSCAR [1, 10-12]. Some mathematical models with analytical solutions have also been developed to predict advection and diffusion of oil concentration in water [18]. Unlike more common surface spills, the Deepwater Horizontal incident happened in June 2010, was the first deepwater spill in which chemical dispersants were directly added to the oil pouring out of the wellhead. So, a new computational model to predict the environmental fate and impact of the marine oil and chemical dispersant was justly developed [16]. However, for the deposition and adsorption of oil by sediment, only a few researches were found, and many other models didn’t consider these processes [2, 3, 6]. For the other chemicals spill into rivers, deposition and adsorption related to sediment is also the process to be discussed. In view of the limited understanding of the chemicals process, the simulations for chemicals spill has room for improvement.

Apart from the understanding of chemical spill process in aquatic environment, how to establish the modeling system for assessing chemicals fate with water flow in the cross-linking river network is also the focus. After all, the current early warning modeling system are usually applicable to the single rivers or open waters, but less efficient in the river network, especially the water system equipped with sluice gates to control water flowing, which decides the chemicals spreading domain.

This paper reports newly developed chemical spill models for simulating the movement of chemicals in plain river network, based on a hydrodynamic model for the river network equipped with sluice gates and a water quality model. Using Shanghai waters as a test bed, the numerical simulations were carried out and the results are verified with observed and experimental data.

II. HYDRODYNAMIC MODEL FOR THE RIVER NETWORK

1. Model Governing Equation

Considering lateral and vertical scale is much smaller than the longitudinal scale in the river network, generally the governing equation of the hydrodynamic model is based on Saint-Venant Eq.:

\[ B \frac{\partial z}{\partial t} + \frac{\partial Q}{\partial x} = q \]  

\[ \frac{\partial Q}{\partial t} + \frac{\partial}{\partial x}(\alpha \frac{Q^2}{A}) + gA \frac{\partial z}{\partial x} + g \frac{n^2 Q^3}{Ah^3} = 0 \]
2. Mode to Control Sluice Gates

Plain river network is usually formed in the coastal region. To prevent flooding from tidal propagation, many sluice gates had been installed in the tidal rivers. In the past, under most circumstances, the sluice gates were closed, as a result the river flowing among the rivers were severed, causing stagnant flow. To augment river flowing with the purpose of improving water quality, dynamic gates operation were implemented, relating to gates control mode with tidal occurrence in the model.

Generally, gate operation is irreversible so as to achieve a unidirectional flow. As shown in Fig. 1, gate’s outside river is a natural tidal river, and gate operation is decided by the water elevation between the inside and outside river. One scenario is that, only when water elevation inside river is higher than that outside river during low tide, gate is opened to achieve a west-east flow, and gate is closed at other time. The other scenario is that, only when water elevation inside river is lower than that outside river during high tide, gate is opened to achieve an east-west flow.

When gate is opened, the discharge across sluice gate is usually computed according to the following equation:

\[
Q_g = C_s B_g \sqrt{2g\left(\zeta_0 - \zeta_s\right)}
\]

(3)

where \(Q_g\) is discharge across sluice gates; \(C_s\) is submerged orifice flowing coefficient; \(B_g\) is lateral gate orifice width; \(\zeta_0\) is gate upstream water depth above gate elevation, that is, \(\zeta_0 = \zeta_u - \zeta_g\); \(\zeta_s\) is gate downstream water depth above gate elevation; \(\zeta_u\) is gate upstream water elevation, \(\zeta_b\) is gate bottom elevation; \(\zeta_i = \zeta_i - \zeta_g\), \(\zeta_i\) is gate downstream water elevation.

When gate is closed, the discharge across the sluice gate is zero.
matter and is transported with it. This particulate matter, along with the sorbed chemical, usually settles onto the bottom of river and forms deposits of contaminated sediments.

In general, the fate of hydrophobic chemicals in the river is determined by partitioning to water and particulate matter, and by transport, as shown in Fig. 3.

The mass conservation equation for the chemical dissolved in water is

\[ \frac{\partial C_d}{\partial t} + \frac{\partial Q C_d}{\partial x} = \frac{\partial}{\partial x} \left( A D \frac{\partial C_d}{\partial x} \right) - k_d k_p \theta C_d - k_s A C_d + k_p k_s \theta A - k_k A C_d \]

where \( C_d \) is the dissolved chemical concentration in water; \( k_d \) is sorption rate; \( k_s \) is desorption rate; \( k_p \) is partition coefficient between suspended sediments and water; \( \theta \) is suspended sediments concentration in water; \( k_b \) is chemical and biological degradation including the process of volatilization, hydrolysis, photolysis, etc.

The mass conservation equation for the chemical sorbed to suspended sediments is

\[ \frac{\partial C_s}{\partial t} + \frac{\partial Q C_s}{\partial x} + P_s w \frac{C_s}{h} A C_s - P_e \frac{E}{h} A C_s = \frac{\partial}{\partial x} \left( A D \frac{\partial C_s}{\partial x} \right) + k_p k_s \theta A C_d - k_s k_p \theta A C_d - k_r A C_s \]

where \( C_s \) is the sorbed chemical concentration in water; \( w \) is settling velocity; \( E \) is re-suspension rate; \( P_s \) is probability for sedimentation, \( P_e = \max(0, 1 - \frac{T_{sed}}{T}) \), \( T_{sed} \) is critical shear stress for sedimentation; \( T \) is ambient shear stress; \( P_r \) is probability for re-suspension, \( P_r = \max(0, \frac{T_{res}}{T} - 1) \), \( T_{res} \) is critical shear stress for re-suspension.

3. Hydrophilic Chemicals Model

Fate and transport of hydrophilic chemicals in water is predominantly determined by advection, turbulent diffusion and bio-chemical degradation, which is described by

\[ \frac{\partial A C}{\partial t} + \frac{\partial Q C}{\partial x} = \frac{\partial}{\partial x} \left( A D \frac{\partial C}{\partial x} \right) - k_b A C \]

where \( k_b \) is boil-chemical degradation. The degradability of hydrophilic chemicals usually decreases as chemicals ages. From a more general level, considering the chemicals in waters include a variety of organic compounds, collective parameters such as chemical oxygen demand (COD), biochemical oxygen demand (BOD), total organic carbon (TOC), particulate organic carbon (POC) or dissolved organic carbon (DOC) are often used to estimate the quantity of these organic matter. A general dissolved oxygen (DO) model is illustrated as Fig. 4.

IV. RESULTS AND DISCUSSION

1. Study Area

Study area is Shanghai river network, covering an area of 6000 km². With Yangtze Estuary to the north, tidal waters propagate into the region via Wusongkou of Huangpu River, as far as Dianfeng (Fig. 5). So, the area is characterized as a tidal river network. Sluice gates were equipped in rivers to control river flowing according to tidal flowing regime in the Huangpu River.

Hydrodynamic model was calibrated with measured data in 2004 in the Huangpu River as well as its tributaries like Suzhou Creek. The calibrated parameter is river’s bottom roughness coefficient, which is calibrated to be in the range of 0.02~0.03. As sown in Fig. 5, Huangpu River is the mainstream...
of this watershed, so calibration of flowing pattern of Huangpu River proves the total tidal flow into the area (Fig. 6). Suzhou Creek is Huangpu River’s largest tributary, which is controlled by sluice gates equipped in the Huangpu River and other rivers (Fig. 7); so, calibration of flowing pattern of Suzhou Creek proves water flowing of this region under sluice gate control (Fig. 8).

In this study, potential chemical spills in Minhang District of Shanghai were assessed, based on the developed hydrodynamic model and chemical spill models. Minhang District is the region abundant in chemical enterprises and rivers, so chemical spill threat to the rivers is of increasing concern. Especially, rivers in this region were refined so as to include any of the potential chemical spills (Fig. 9).

2. Oil Spill Scenario

Oil and its refinery products are the most common potential risks in this area, which are usually generalized as the mixture of the components including alkane, cycloparaffins, mononuclear aromatics, naphthalenes, etc. The processes in the oil spill model are presented in Table 1 based on the parameters verification from a series of studies [4, 19].
Fig. 9. Refined water courses in Minhang District of Shanghai.

Table 1. Oil parameters and some parameters in the oil spill model.

<table>
<thead>
<tr>
<th>Properties of Oil</th>
<th>Parameters</th>
</tr>
</thead>
<tbody>
<tr>
<td>Oil type</td>
<td>Crude oil</td>
</tr>
<tr>
<td>Oil density</td>
<td>850 kg/m³</td>
</tr>
<tr>
<td>Oil kinematic viscosity</td>
<td>50 cSt</td>
</tr>
<tr>
<td>Oil maximum water content</td>
<td>1.0</td>
</tr>
<tr>
<td>Wind drag coefficient</td>
<td>0.03</td>
</tr>
<tr>
<td>Horizontal diffusion coefficient</td>
<td>5 m²/s</td>
</tr>
<tr>
<td>Minimum thickness</td>
<td>0.5 mm</td>
</tr>
<tr>
<td>Evaporation rate</td>
<td>0.4 d⁻¹</td>
</tr>
<tr>
<td>Dispersion rate</td>
<td>Calculated</td>
</tr>
<tr>
<td>Oil settling velocity</td>
<td>Calculated</td>
</tr>
</tbody>
</table>

Settling velocity of oil droplet is calculated based on Stokes Equation:

\[ w_s = \frac{1}{18} \frac{\rho_o - \rho_w}{\mu_w} g d^2 \]  (9)

where \( \rho_o \) is oil density; \( \rho_w \) is water density; \( \mu_w \) is water viscosity; \( d \) is oil diameter, \( d = 100 \mu m \). Based on Eq. (9), it is calculated that settling velocity of oil droplet is \( 1.25 \times 10^{-4} \) m/s.

Dispersion rate of oil droplet is calculated based on the equation as follows:

Fig. 10. Oil movement and oil concentration on water surface of study domain.
\[ Q = \int_{d_{\text{min}}}^{d_{\text{max}}} Q(d) \Delta d \]  

(10)

\[ Q(d) = C^\prime d^{3.57} F_{\text{w}} N_0 d^{0.7} \]  

(11)

\[ D_e = 0.000584 \rho_s U_w^2 \]  

(12)

\[ F_{\text{w}} = \frac{\max(0, 0.032(U_w - 5.0))}{8.13 U_w / g} \]  

(13)

where \( Q \) is dispersion rate; \( Q(d) \) is dispersion rate of oil particles with particle sizes in an interval \( \Delta d \) around \( d \); \( N_0 \) is normalisation constant distribution function; \( d_{\text{min}} \) is minimal oil droplet diameter; \( d_{\text{max}} \) is maximal oil droplet diameter; \( C^\prime \) is oil constant relating to oil kind; \( D_e \) is wave energy dissipation per unit surface area; \( F_{\text{w}} \) is number of waves that break per unit surface area; \( \rho_s \) is water density; \( U_w \) is wind speed.

The following conditions were considered in the oil spill simulation:

Type of oil: 1 tons crude oil;
Simulation period: two days;
Wind: Southeast wind with the speed of 4.0 m/s;
Water flowing pattern: Based on the developed hydrodynamic model, the flowing field of the simulation area can be obtained;
Oil process: Based on the process described in Table 1.

Oil spreading and oil concentration on water surface is shown in Fig. 10. It can be seen that oil spreads with water flowing and wind, but oil concentration becomes smaller with time due to its strong evaporation. After 12 hours of sudden discharge, oil concentration on water surface is less than 0.001 mg/L, while oil spreading domain decreases gradually.

Oil dispersed in water can be excluded from consideration. The reason is that oil dispersion rate is insignificant, which is less than \( 10^{-3} \) in the simulation scenario.

3. Hydrophobic Chemical Spill Scenario

In this paper, potential HCB discharge was assessed. The parameters used in the model are presented in Table 2 based on the parameters verification from a series of studies [5, 8, 17].

Volatilization rate is based on the double film theory, which can be defined as

\[ \frac{1}{k_v} = \frac{1}{k_L} + \frac{RT}{k_g k_H} \]  

(14)

where \( k_v \) is volatilization rate; \( k_L \) is transfer coefficient for the hydrophobic chemicals for the liquid film; \( k_g \) is transfer coefficient for the hydrophobic chemicals for the gas film; \( k_H \) is Henry’s constant, \( k_H = 70 \) Pa m³/mole; \( T \) is absolute water temperature (K), \( R \) is gas constant.

\[ k_v = 273.15 \times (U_w + U) \times \frac{18}{\sqrt{M_w}} \]  

(15)

\[ k_L = 5.64 \times \left( \frac{U^{0.966}}{H^{0.821}} \right) \times \frac{32}{\sqrt{M_w}} \times e^{(0.526(U - 1.9))} \]  

(16)

where \( H \) is water depth; \( M_w \) is molecular weight; \( U \) is water flowing velocity.

The following conditions were considered in the HCB spill simulation:

Quantity of HCB: 1 tons;
Simulation period: two days;
Water flowing pattern: Based on the developed hydrodynamic model, the flowing field of the simulation area can be obtained;
HCB process: Based on the process described in Table 2. HCB process is simulated as dissolved HCB and particulate HCB respectively.

Fate and transport of dissolved HCB and particulate HCB in the rivers is shown in Fig. 11 and Fig. 12. It can be seen that concentration of particulate HCB increases with time due to its larger partition coefficient on the order of \( 10^6 \) L/kg. At the same time, the particulate matter, along with the sorbed HOC, also settles onto the bottom of an aquatic system and forms deposits of contaminants. Because of its biochemically refractory character in water, in the relatively long term, dissolved HCB concentration as well as particulate HCB concentration is larger than the oil concentration on the water surface under same discharge quantity for the simulation.

<table>
<thead>
<tr>
<th>Properties of HCB</th>
<th>Parameters</th>
</tr>
</thead>
<tbody>
<tr>
<td>HCB density</td>
<td>2440 kg/m³</td>
</tr>
<tr>
<td>Horizontal diffusion coefficient</td>
<td>5 m²/s</td>
</tr>
<tr>
<td>Partition coefficient (Log form)</td>
<td>6.41 L/kgC</td>
</tr>
<tr>
<td>Settling velocity</td>
<td>2.0 × 10⁻¹ m/s</td>
</tr>
<tr>
<td>Re-suspension rate</td>
<td>0.1 g/m²/s</td>
</tr>
<tr>
<td>Critical shear stress for sedimentation</td>
<td>0.2 N/m²</td>
</tr>
<tr>
<td>Critical shear stress for re-suspension</td>
<td>0.3 N/m²</td>
</tr>
<tr>
<td>Sediment concentration</td>
<td>30 mg/L</td>
</tr>
<tr>
<td>Adsorption rate</td>
<td>0.42 d⁻¹</td>
</tr>
<tr>
<td>Desorption rate</td>
<td>0.10 d⁻¹</td>
</tr>
<tr>
<td>Volatilization rate</td>
<td>Calculated</td>
</tr>
</tbody>
</table>

Table 2. HCB properties and some parameters used in the hydrophobic chemical spill model.
scenarios. So, it is suggested that PCB transport in waters should be blocked as quickly as can after its discharge.

V. CONCLUSION

An early warning modeling system for tidal river network region has been developed to simulate the fate and transport of chemicals in rivers from a potential sudden chemical discharge.

To assess chemicals transport in rivers, a hydrodynamic model was firstly developed to simulate river flowing field under rivers junction and artificial sluice gates control. Compared with the observed data of Huangpu River and Suzhou Creek, the numerical results of the hydrodynamic model show good conformity.

Further, according to chemical properties, three kinds of water quality models including oil spill model, hydrophobic chemical model, and hydrophilic chemical model were developed. Oil spill model is capable of predicting the horizontal movement of surface oil slick and oil particle concentration distribution in water body. Hydrophobic chemical model is capable of predicting fate of chemicals in rivers dependent on the adsorption to sediments with sedimentation and re-suspension, as well as chemical and biological process. Hydrophilic chemical model is capable of predicting fate of organic compounds in rivers relating to chemical and biological degradation. The hydrodynamic model and three kinds of water quality models form an integrated modeling system to assess potential river water quality threat from sudden chemical discharge accidents in plain river network region.

Using Shanghai waters as a study area, two chemical spill scenarios including potential oil spill and HCB spill as hydrophobic chemical were simulated to display the application of early warning modeling system, based on the calibration of model parameters. The authors will collect more field measurements of sudden chemical discharge accidents to refine the developed modeling system.

Fig. 11. Fate and transport of dissolved HCB in the rivers of study domain.
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REFERENCES


